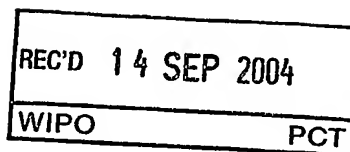


PRVPATENT- OCH REGISTRERINGSVERKET
Patentavdelningen**Intyg
Certificate**

Härmed intygas att bifogade kopior överensstämmer med de handlingar som ursprungligen ingivits till Patent- och registreringsverket i nedannämnda ansökan.

This is to certify that the annexed is a true copy of the documents as originally filed with the Patent- and Registration Office in connection with the following patent application.



(71) Sökande Kerttu Eriksson, Essex C03 3QR GB
Applicant (s)

(21) Patentansökningsnummer 0302277-9
Patent application number

(86) Ingivningsdatum 2003-08-21
Date of filing

Stockholm, 2004-08-24

För Patent- och registreringsverket
For the Patent- and Registration Office

Bibi Skripe
Bibi Skripe

Avgift
Fee

PRIORITY DOCUMENT
SUBMITTED OR TRANSMITTED IN
COMPLIANCE WITH
RULE 17.1(a) OR (b)

BEST AVAILABLE COPY

2003 -08- 2 1

Huvudfaxen Kassin

APPLICANT:

KERTTU ERIKSSON

TITLE:

METHOD AND APPARATUS FOR DEHU-
MIDIFICATION

5

Technical Field

The present invention concerns a method and an apparatus for dehumidifying, drying or the like of many different types of material. The material for dehumidifying or the like may be chemical and organic materials, such as sewage sludge, colour, foodstuffs, parts of humans or animals.

15

Prior Art

The present invention is based on the concept of employing thermal radiation.

Thermal radiation has the characteristic property that it requires no medium for transferring energy between two bodies. This may be likened to the energy of the sun, which is conveyed to the earth.

Radiation having relatively short wavelengths will penetrate into openings of the surface layer of the material to be dehumidified, dried or the like. The radiation going through these openings will be reflected multiple times from moisture molecule to moisture molecule. If the moisture is absorbent enough, the likelihood is low that any part of the radiation will go out through the openings formed in the molecular structure of the material. Thus, the material will form a black surface.

30

The above process may be named "radiation of void", thus applying for radiation having wavelengths shorter than the openings of the surface structure. Due to the small openings in the molecular structure of the material to be dehumidified the radiation will be isotropic, i.e. the intensity is the same in all directions.

35

In the inner part of the material to be dehumidified and having its voids the radiation will have the spectral distribution described by Kirchhoff's law:

$$\frac{e_1(\lambda, T)}{a_1(\lambda, T)} = \frac{e_2(\lambda, T)}{a_2(\lambda, T)} = \dots e_r(\lambda, T)$$

- 5 and Stefan-Boltzmann's law regarding the total intensity:

$$E_r = \int e_r(\lambda, T) \cdot d\lambda = \sigma \cdot T^4$$

- 10 The present invention is mainly developed for treatment, i.e. dehumidification, sanitation or drying, of sewage sludge, but a person skilled in the art realises that it may be used for many different materials.

The present invention is also appropriate for dehumidification or drying of some foodstuffs. Suitable foodstuffs may be crispbread, pasta etc.

- 15 In order to simplify the description the invention will be described mainly with sewage sludge as an example. If at all treated sewage sludge at the present is often heated to rather high temperatures in the region of 800-900 °C. Such high temperatures make demands on the apparatus
20 used, especially the vessel holding the sludge during heating. However, sewage sludge is normally just used for land-filling or deposition.

Summary of the Invention

- 25 The present invention is based on the concept of only employing radiation energy (thermal radiation) for heating the sludge or other material and that the radiation employed encompasses a wave length range within which water has a high absorption coefficient. The radiation at other
30 wavelengths is reduced.

A heat source is used to emit heat radiation. Vaporised moisture will be taken away by circulating air from the surface of the material to be dehumidified. The vapor-

2003-08-21

Huvudfaxen Kassan

sation of moisture of the material is done by means of absorption and reflection. The heat source will emit heat radiation at wavelengths at which water has high capacity of absorption, with absorption coefficients larger than 1000 cm⁻¹.

5 With radiation energy in a narrow wavelength band where the water has a high absorption capability, the radiation energy is transmitted direct to the water molecules in the material to be dehumidified. This result in relatively short drying times, relatively low energy consumption and normally no negative influence on the material to be dehumidified. Dehumidifying using "the void principal" as indicated above will give a low consumption of energy.

10 For sewage sludge the moisture ratio after drying should be 20% or less. By using the method of the present invention the moisture ratio may be decreased well below 20%. In the drying process the sludge will also be sanitised to a certain degree. As the sludge is heated to 70-120 °C in the process most bacteria of the sludge will be killed. The sanitised sludge may be recycled, i.e. it may be placed on e.g. fields for standing crops.

15 The method of the present invention can be used as a part of an ecological system of recycling. By such a system a number of advantages may be reached. The dried and sanitised material, such as sewage sludge may be deposit or burned. The amount of refuse is reduced, decreasing the use of resources. If the dehumidified sludge is burned different materials may be recovered, saving resources and energy compared to using fresh raw material. It is possible to recover heavy metals, chromium, nickel, copper etc. from the ash after burning. It is possible to recover plant nutrients, such as phosphorous being a limited resource, for use in the cultivation of plants. The dehumidified and sanitised sludge normally has a high energy value, e.g. 2.5-3.5 MWh/ton. Thus, it may be used as fuel.

2003-08-21

Huvudfaxen Kassan

Brief Description of the Drawings

Fig. 1 is a perspective view of a drying chamber according to the present invention.

5 Fig. 2 is a sectional side view of a modified chamber according to the present invention.

Fig. 3 is an "open" end view in sketch form of a chamber according to the present invention.

10 Fig. 4 is a sectional view of one example of a heat source to be used in the chamber of the present invention.

Detailed Description of Preferred Embodiments

15 Figs. 1-3 show one embodiment of a drying apparatus including a drying chamber 1 in which the drying of the sludge or other material takes place.

The expression "element" 2 will be employed below to refer to a radiation source. The element is designed as a device emitting radiation comprising a selected wavelength region. In one embodiment the elements 2 are made of a central electric resistor 15 surrounded by a tube 14. In other
20 embodiments the electric resistor is replaced by hot water as the radiation source of the element 2. Also other energy media is possible to use as the radiation source. Independent of which energy media that is used, it should be surrounded by a tube 14. Furthermore, the energy medium may be
25 made more effective by the use of a plasma or a dielectric.

The elements 2 may be placed in racks or frames 12. Reflectors are normally placed in connection with the elements. In order to realise good reflection of the radiation, the reflectors are generally made of aluminium,
30 stainless steel or other high-reflective material. In the frequencies employed, these materials display reflection coefficients exceeding 95%. Radiation which impinges on the reflectors is guided by them back to the sludge. It is not
35 a requirement that reflectors are employed, but they do

2003 -08- 2 1

Huvudfaxen Kåsson

contribute to a reduction in energy consumption. Normally, the elements 2 are disposed in any optional direction whatever in relation to the longitudinal direction of the drying chamber 1.

5 As a rule, the walls of the chamber are clad on the inside with stainless and/or acid proof steel, aluminium or similar high-reflective material for radiation within the above-indicated selected wavelength region. In other words, the interior of the drying chamber is designed as a large
10 reflector. The walls are generally thermally insulating. As shown in Fig. 1 a door 21 is arranged at each end of the chamber 1. In other embodiments there is a door 21 only at one end of the chamber 1, in which case the sludge 7 or other material is taken in and out of the chamber 1 at the
15 same end.

The sludge 7 is normally received on a conveyor belt 13. In some embodiments a conveyor belt 13 of stainless steel is used to support the material to be dehumidified, reflecting some radiation back to the sludge 7. In some em-
20 bodiments the conveyor belt 13 is made of a net of wires of stainless steel or the like. If the conveyor belt has a mesh form some elements 2 are placed in the centre of the conveyor, i.e. between the upper and lower horizontal parts of the conveyor. In other embodiments the sludge 7 is re-
25 ceived on one or more carriages, that may be rolled into and out of the drying chamber 1. Also the carriages may have sludge receiving surfaces of a high reflective material, such as stainless steel. If a conveyor belt 13 is arranged in the chamber 1, the sludge 7 is normally feed in
30 at one end of the conveyor and feed out at the other end. During the dehumidification process the conveyor belt is normally at a standstill.

The drying chamber 1 is normally placed on legs 19. The drying chamber 1 is, in the illustrated embodiment,
35 provided with a circulation fan 4 and a ventilation damper

2003-08-21

Huvudfaxen Kassar

11. An air inlet 16 and an air outlet 17 are placed at opposite ends of the chamber 1. Both the air inlet 16 and the air outlet 17 are normally furnished with dampers, to open and close the inlet 16 and outlet 17, respectively. Normally, the areas of the air inlet and outlet, respectively, are separated from the proper drying chamber 1 by partitions 20. The partitions 20 normally have openings for the conveyor belt 13. Furthermore, a conduit 3 for recirculation of air is provided, giving recovery of energy. A heat exchanger 18 is placed in the conduit 3 for recirculation. The conduit 3 including the heat exchanger 18 makes it possible to dehumidify and recirculate the air of the drying chamber. Furthermore dampers 11 are placed at each end of the conduit 3.

15 In one embodiment, as indicated in Fig. 2 the active part of the circulation fan 4 is placed in the conduit 3. In other embodiments, as indicated in Fig. 1, the active part of the circulation fan 4 is placed inside the chamber 1. The circulation fan 4, irrespective of the exact placing, circulates the air in the drying chamber 1 and thereby conveys off moisture, which departs from the surface of the sludge 7. The task of the fan system is to circulate the air around the sludge and thereby entrain moisture from the surface of the sludge. In the present invention, use is normally made of a flow rate of 1-5 m/s.

The ventilation damper 11 is employed for regulating the air velocity and the speed of dehumidification in the drying chamber 1. In some embodiments there are more than one damper 11.

30 In the drying apparatus, there is disposed an indicator 5 for measuring the temperature in the drying chamber 1 and/or of the air which departs from and/or is fed to the drying chamber 1. Also the temperature of the sludge 7 may be controlled. Different indicators for different temperatures may be used, measuring both the "wet" and "dry" tem-

2003-08-21

Huvudföreläsaren Kassar

peratures. For a "wet" thermometer water is cooled by evaporation until equilibrium, i.e. the heats of evaporation and volatilisation are the same. The dampers 11 of the chamber 1 may be controlled by the wet temperature. Normally an indicator 9 measuring the temperature of the sludge 7 is used. Said indicator 9 is placed in the sludge 7. In certain embodiments, there are also indicators 6, which measure the moisture ratio of the drying chamber 1. For accurate monitoring of the air humidity in the chamber, use is made of indicators 6 that measure the relative air humidity. As indicator for the relative air humidity a psychrometer is used in some embodiments. In order to measure the decrease of the moisture in the sludge 7, use is made, in certain embodiments, of a weighing machine. The weighing may be performed in that the chamber is placed on scales or load sensing elements 10. Said scales or load sensing elements 10 are in some embodiments integrated in the legs 19 on which the chamber 1 is placed.

In some embodiments of the present invention a condenser 8 placed below the conveyer belt 13 is used. By means of the condenser 8 some energy is recovered.

As stated above drying of the sludge 3 takes place with the aid of the elements 2. These elements 2 emit a radiation in a limited wavelength interval adapted to the absorption of water.

In the embodiment according to Fig. 4, the element 2 consists of an electric resistor 15 disposed centrally in the tube 14 and heated when current from a voltage source passes through the resistor via conductors (not shown).

The wavelength band has been selected at the range of approx. 2-20µm and as a rule approx. 5-20µm, a range that encompasses wavelengths at which the absorption of radiation by water is great. In such instance, use is made of the fact that, within these ranges, water has peaks with absorption coefficients higher than 1,000 cm⁻¹.

2003-08-21

Huvudföreläsaren Kassar

The water has peaks at approx. 3µm, 6-7µm and 10-20µm regarding the absorption. Between approx. 7µm and 10µm the absorption coefficient of water is lower, sinking under 1,000 cm⁻¹. Thus, to maximise the effect of the radiation of the elements 2, they should have maximal intensity at the frequencies where water has maximal absorption, while the radiation at other wavelengths should be reduced.

Thus, one object of the present invention is to have a radiation with maximal intensity at the wavelengths where water has a high absorption coefficient, while the intensity is reduced at other wavelengths. The peak at 3µm is rather thin and demands a very high temperature making it less suitable to use. Furthermore, it is very hard and even virtually impossible, to reduce the radiation at the wavelength range approx. 4-6µm. In view of this the intensity of the radiation of the elements is directed to the intervals approx. 6-7µm and 10-20µm and the intensity is reduced in the intermediate area, i.e. approx. 7-10µm. Thus, the energy of the radiation is used in a way to give maximal effect.

The intensity is dependent on the material of the elements according to the following formula:

$$I=I_0e^{-\alpha x}$$

where I is the intensity, e is the natural logarithm and α is a constant depending on the material of the tube 14 or the like surrounding the resistor 15. By varying the material it is possible to control both the spectrum and the position of the radiation of the elements 2. This is used according to the present invention in such a way that the radiation of the elements 2 are adapted to the absorption of water as indicated above. Thus, according to the present invention the material surrounding the electrical resistor 15 is chosen to give the desired radiation spectrum of the element 2. Said material may be any material giving the desired properties. According to known technol-

2003-08-21

Huvudförfattaren Kossan

ogy, there is a plurality of examples of how, by suitable material selection and suitable current force, to obtain the working temperature of the radiation source which entails that the radiation is maximised within the wavelength interval at which water best absorbs radiation.

Normally the conveyor belt 13, and thus, the sludge 7, is at standstill during the treatment phase. The treatment phase is normally an automated process, controlled by use of one or more of the different indicators referred to above. The process may be controlled using either the moisture ratio of the chamber 1 or sludge 7, or time as independent variable. By using a thermometer in the circulating air or the sludge 7 dehumidification may be conducted at a certain temperature level of the chamber 1 or sludge 7, respectively. A combination of these temperatures may be used as depending variables.

Usually a control system (PLC system) is provided for controlling the elements 2, the fan 4 and the damper 11 in response to signals received from the indicators 5, 6, 9, 10. The control system may also be referred to as a registration and calculation unit. Normally the process is run automatically, but a person skilled in the art realises that the process may also be run manually by continuous monitoring of the values of the indicators 5, 6, 9.

The temperature in the drying chamber 1 is governed with the aid of the elements 2. In the process often the temperature of the sludge 7 is kept at a fixed level (e.g. ± 1 °C). It is also possible to keep the temperature of the chamber 1 at a fixed level. To keep any of said fixed temperature levels the elements 2 are turned on and off based on the temperature of the sludge 7 or chamber 1, respectively. For treatment of sewage sludge the air temperature in the chamber 1 is kept at about 150 °C and the temperature of the sewage sludge is held at about 50-120 °C. The process goes on until the moisture ratio of the sludge 7

2003-08-21

Huvudföreläsning Kassar

has decreased into a predetermined level. As an alternative to the moisture level the process may be run for a predetermined time. To kill of bacteria the temperature of the sludge 7 may be raised for a short period, usually in the end of the process.

After the dehumidification process the sludge 7 is treated whether any material are to be recovered before or after a possible burning, whether it should be spread on the ground, whether it should be used as a fuel etc.

A drying process for foodstuffs, such as crispbread, pasta etc., is run after the same principals as described above. The type and number of indicators used will be adapted to the material to be dried.

030820 LK G:\HEM\PAT\LK\Foc\US040002_PatentText.doc

11

Ink. t. Patent och T. T. T.

2003-08-21

Hörselörens Kassa

CLAIMS

1. A method for dehumidifying, drying or the like of different material in a drying chamber (1), **characterized** in that thermal radiation is used concentrated to one or more distinct wavelength ranges at which water has peaks for absorption of radiation energy and that air is circulated in the chamber (1) to take up moisture evaporated from the material.
2. The method of claim 1, **characterized** in that at least one element (2) is disposed in the drying chamber emitting thermal radiation and that emitted radiation is concentrated to exact wavelength ranges where the water has an absorption coefficient greater than approx. $1,000\text{cm}^{-1}$, while the radiation is reduced in other areas.
3. The method of claim 1 or 2, **characterized** in that the radiation is concentrated to the wavelength ranges of approx. $6-7\mu\text{m}$ and approx. $10-20\mu\text{m}$, while the radiation in the intermediate range, i.e. approx. $7-10\mu\text{m}$ is reduced.
4. The method of any of the previous claims, **characterized** in that the prevailing moisture ratio and/or the temperature of the material and/or the chamber (1) is monitored.
5. The method of claim 4, **characterized** in that the moisture ratio of the material and/or the chamber is monitored by means of one or more indicators (6, 9).
6. The method of claim 4, **characterized** in that the moisture ratio of the material and/or the chamber is monitored by means of a weighing machine (10), monitoring the total weight of the chamber (1).
7. The method of any of the preceding claims, **characterized** in that the air of the chamber is circulated by means of a fan (4), an air inlet (16) placed at one end of the chamber (1) and an air outlet (17) placed at an opposite end of the chamber; that the air is recirculated by means of a conduit (3) going from one end of the chamber

030920 IK G:\MEM\PAT\IK\Doc\U5040002_Patenttext.doc

12

Ink. t. Patent- och reg.verket

2003-08-21

Huvudfaxen Kassin

(1) to the opposite end; that a heat exchanger (18) is placed in the conduit (3); that one or more dampers (11) are arranged to let out air from the chamber (1); and/or that a condenser (8) is placed in the chamber (1).

5 8. The method of any of the preceding claims, **characterized** in that the material to be dehumidified etc. is received on a conveyor belt (13) inside the chamber (1).

10 9. The method of any of the claims 1 to 7, **characterized** in that the material to be dehumidified is received on one or more carriages.

15 10. The method of claim 8 or 9, **characterized** in that the thermal radiation is reflected on high-reflective material on the inside of the chamber (1) and on the surface of the conveyor belt (13) or the carriages receiving the material.

11. The method of any of the preceding claims, **characterized** in that it is used for dehumidification and/or sanitation of sewage sludge (7).

20 12. The method of claim 11, **characterized** in that the sewage sludge (7) is kept at a constant temperature in the interval range of 70-120 °C during the humidification cycle.

25 13. The method of claim 11 or 12, **characterized** in that it is used as a part of an ecological system of recycling.

14. The method of any of the claims 1 to 10, **characterized** in that it is used for drying of foodstuffs, such as crispbread or pasta.

30 15. An apparatus for dehumidification, drying or the like in accordance with the method as claimed in any of the preceding claims, **characterized** in that it comprises a drying chamber (1) including at least one element (2) disposed in the drying chamber for emitting thermal radiation; that a fan (4) is provided for the circulation of air in the
35 drying chamber; that indicators (5, 6, 9) are provided for

2003-08-21

Huyudförsen Kassan

sensing the temperature and/or moisture ratio of the chamber (1) and/or the material to be dehumidified; dried or the like; and that a control system (PLC system) is provided for controlling the elements (2) and the fan (4) in response to signals received from the indicators (5, 6, 9).

16. The apparatus of claim 15, **characterized** in that the elements (2) are mounted in racks (12) and that the racks (12) have surfaces displaying high reflectance.

17. The apparatus of claim 15 or 16, **characterized** in that the drying chamber (1) is constructed from a chamber which, on the inside, is made of or clad with a material displaying high reflectance; that the drying chamber (1) is provided with an air inlet (16), an air outlet (17), a fan system (4), a conduit (3), including a heat exchanger (18), for recirculation of the air of the chamber (1) and one or more ventilation dampers (14); that indicators (9, 10) are provided for sensing temperature and air humidity in the drying chamber (1); that indicators (27) are provided for sensing the weight of the wood; and that the signals from all indicators (7-10, 27) are fed to a calculation and control device (12).

18. The apparatus of any of the claims 15 to 17, **characterized** in that a conveyor belt (13) and/or a condenser (8) is placed inside the chamber (1).

19. The apparatus of any of the claims 15 to 18, **characterized** in that each element (2) comprises an electrical resistor (15) surrounded by a tube (17) or the like and/or that the part surrounding the electrical resistor (15) is made of material having properties to give the desired radiation spectrum.

2003-08-21

Huvudförf. Kassar

ABSTRACT

The present invention concerns a method and apparatus for dehumidifying, drying or the like of different materials. The invention is developed primarily for dehumidification of sewage sludge (7), but it may be utilised for many different materials including foodstuffs as crispbread and pasta. The sludge (7) or other material is dehumidified or dried in a chamber (1) by means of thermal radiation. The thermal radiation is given by means of one or more elements (2) for thermal radiation. The thermal radiation is concentrated to one or more distinct wavelength ranges at which water has peaks for absorption of radiation energy. Air is circulated in the chamber (1), to take up moisture evaporated from the material.

To be published with Fig. 2.

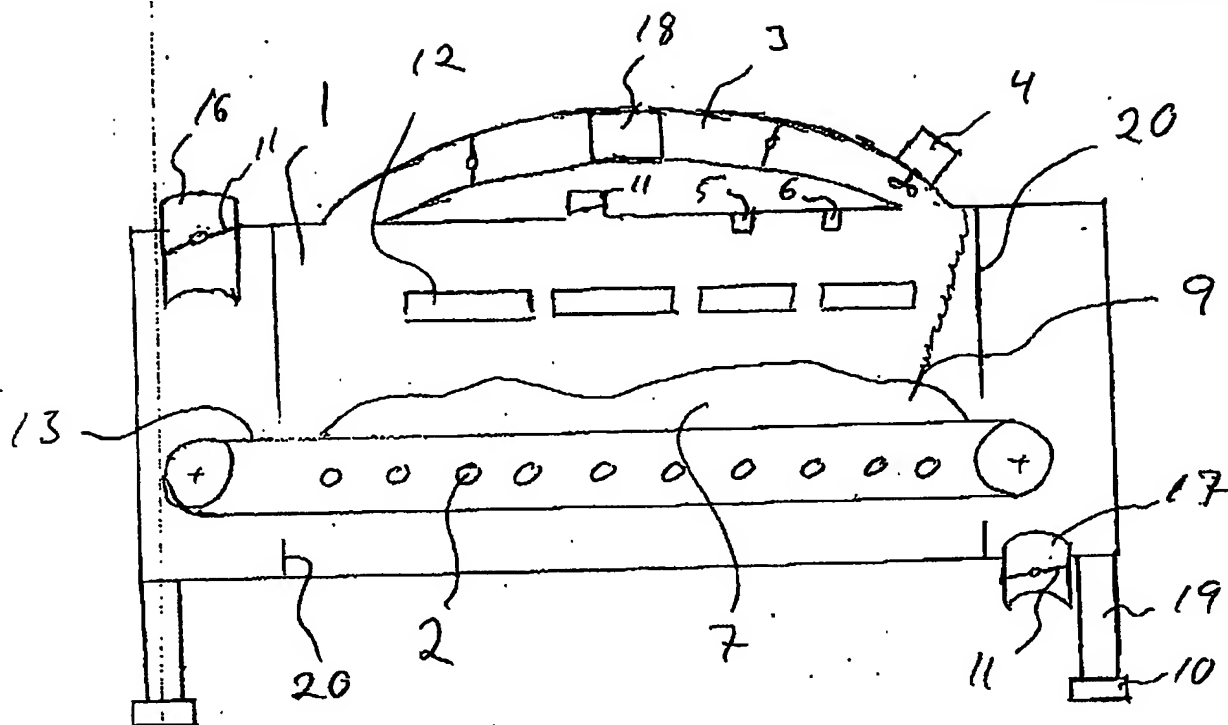


Fig. 2

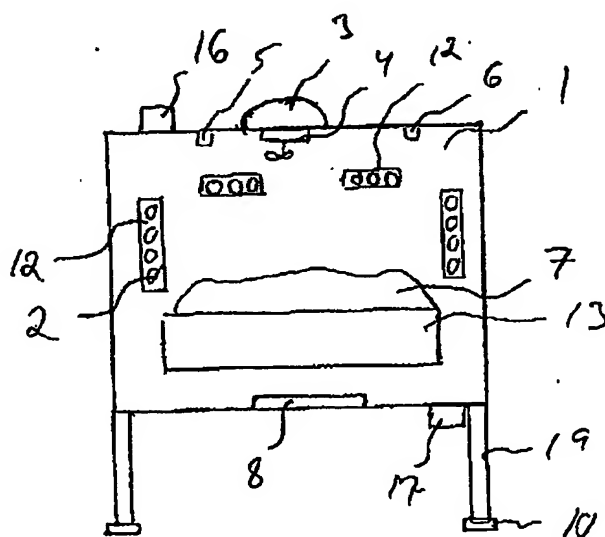


Fig. 3

Ink. t. Patent- och reg.

2003-08-21

Huvudföretag Kass

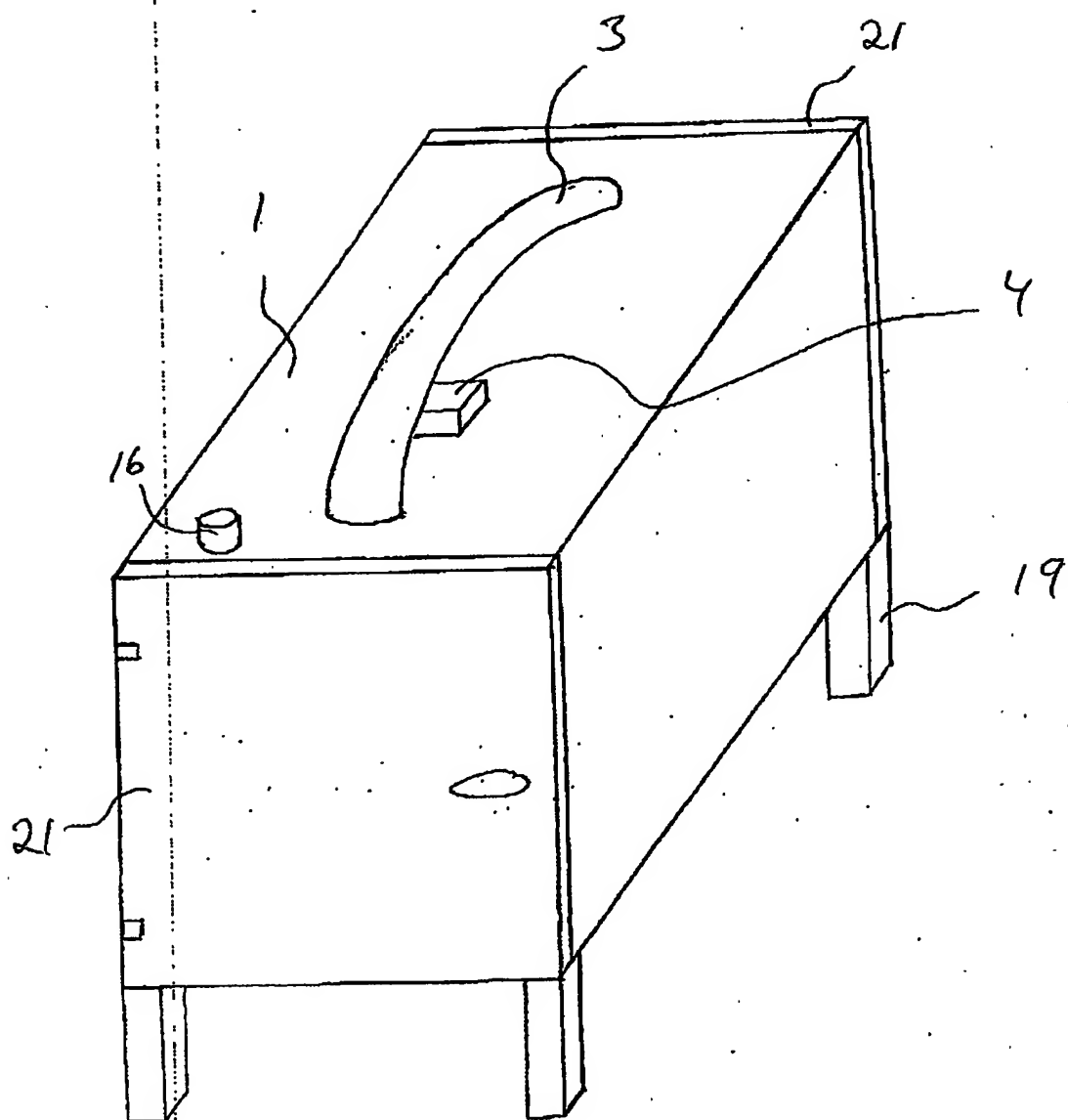


Fig. 1

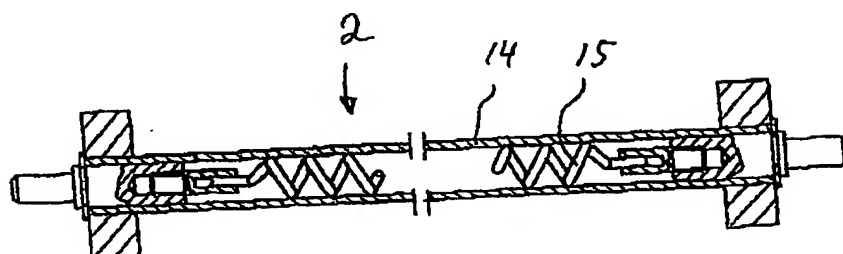


Fig. 4

**This Page is Inserted by IFW Indexing and Scanning
Operations and is not part of the Official Record**

BEST AVAILABLE IMAGES

Defective images within this document are accurate representations of the original documents submitted by the applicant.

Defects in the images include but are not limited to the items checked:

- ☒ **BLACK BORDERS**
- ☐ **IMAGE CUT OFF AT TOP, BOTTOM OR SIDES**
- ☐ **FADED TEXT OR DRAWING**
- ☐ **BLURRED OR ILLEGIBLE TEXT OR DRAWING**
- ☐ **SKEWED/SLANTED IMAGES**
- ☒ **COLOR OR BLACK AND WHITE PHOTOGRAPHS**
- ☐ **GRAY SCALE DOCUMENTS**
- ☐ **LINES OR MARKS ON ORIGINAL DOCUMENT**
- ☐ **REFERENCE(S) OR EXHIBIT(S) SUBMITTED ARE POOR QUALITY**
- ☐ **OTHER:** _____

IMAGES ARE BEST AVAILABLE COPY.

As rescanning these documents will not correct the image problems checked, please do not report these problems to the IFW Image Problem Mailbox.